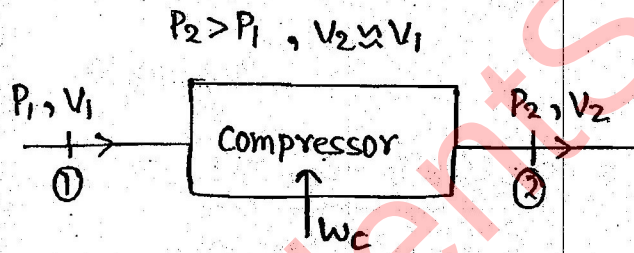


# COMPRESSOR →



The function of a compressor is to increase the pressure of gas and vapour from lower to higher pressure and for that work is done from outside.

## Classification :-

Based upon working principle :-

1) Positive Displacement compressor :-

In these compressor the pressure of gas is increased by decreasing its volume in a confined cylinder i.e. rise in

In compressor →  $T$  changes

In pump →  $T$  (No change)  
(incompressible)  
∴ water is used

⇒ If water is supplied in pump to the compressor then theoretically is possible but practically is not possible because

compressor blade is light and easily breakable but pump blade is robust in design means hard.

● pressure is obtained by positively displacement fluid to lower volume.

● Ex → Reciprocating compressor.

● (b) Dynamic compressor :-

● In these compressor high kinetic energy is given to fluid by a rotating element called rotor and then this high kinetic energy is converted into pressure energy in the diffuser. That is rise in pressure is obtained due to dynamic action of gas.

● Ex → Centrifugal and axial compressor.

● (2) Based on pressure developed :-

● (i) Low pressure → 10 bar

● (ii) Medium pressure → 10 bar to 80 bar

● (iii) High pressure → above 80 bar.

● (3) Based on pressure Ratio ( $P_r = P_2/P_1$ ) :-



● (i) Fan →  $1.0 < P_r < 1.1$

● (ii) Blower →  $1.1 < P_r < 2.3$

● (iii) Compressor →  $P_r > 2.3$

● (4) Based on Volume Handling ( $m^3/sec$ ) or ( $m^3/min$ ) :-

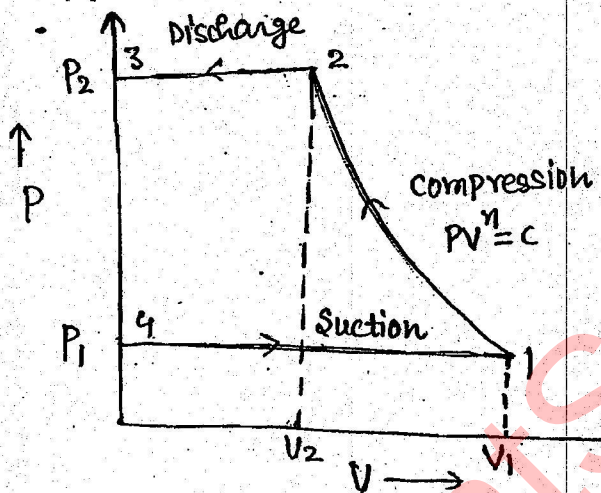
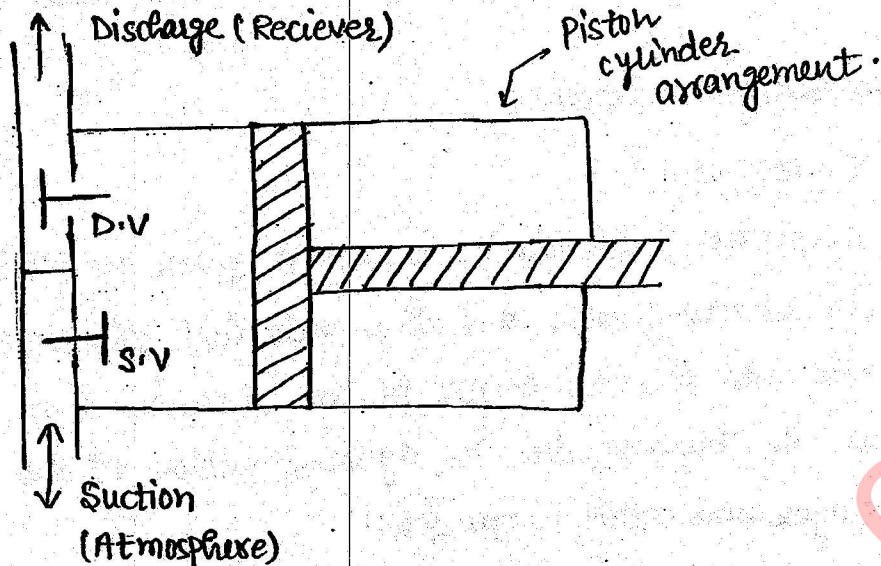
● (i) Small → upto  $9 m^3/min$

● (ii) Medium → 9 to  $3000 m^3/min$

● (iii) Large → above  $3000 m^3/min$



## RECIPROCATING COMPRESSOR



⊕ Reciprocating Compressors are able to produce very high pressure but the volume delivered is very less and there is problem of intermittent supply and poor efficiency. In construction it consists of two piston cylinder arrangement with two valves one on the

suction side and other on the discharge side. These are simple automatic valves which work due to pressure difference across the valve.

These compressors are used in Air conditioners, Refrigeration systems, Mining work, air filling station, air motor, drilling, chemical factories etc.

Work input required without clearance volume :-

Workdone per cycle is given by area 1-2-3-4-1.

Workdone by air during suction (4-1),  $w_s = P_1(V_1 - 0) = P_1 V_1$



workdone on air during compression (1-2),

$$w_c = \frac{P_1 V_1 - P_2 V_2}{n-1} = \frac{-(P_2 V_2 - P_1 V_1)}{n-1}$$

workdone on air during discharge, (2-3),  $w_d = P_2 (V_3 - V_2) = -P_2 V_2$

$$w_{\text{cycle}} = - \left[ P_2 V_2 - P_1 V_1 + \frac{P_2 V_2 - P_1 V_1}{n-1} \right] = -(P_2 V_2 - P_1 V_1) \frac{n}{n-1}$$

As compressor work is always -ve, so taking only the magnitude.

$$w_{\text{cycle}} = \left( \frac{n}{n-1} \right) (P_2 V_2 - P_1 V_1)$$

$$w_{\text{cycle}} = \left( \frac{n}{n-1} \right) P_1 V_1 \left[ \frac{P_2}{P_1} \frac{V_2}{V_1} - 1 \right]$$

process, 1-2  $\rightarrow P_1 V_1^n = P_2 V_2^n \Rightarrow \frac{V_2}{V_1} = \left( \frac{P_1}{P_2} \right)^{\frac{1}{n}} = \left( \frac{P_2}{P_1} \right)^{-\frac{1}{n}}$

$$w_{\text{cycle}} = \left( \frac{n}{n-1} \right) P_1 V_1 \left[ \frac{P_2}{P_1} \left( \frac{P_2}{P_1} \right)^{-\frac{1}{n}} - 1 \right]$$

$$w_{\text{cycle}} = \left( \frac{n}{n-1} \right) P_1 V_1 \left[ \left( \frac{P_2}{P_1} \right)^{\frac{n-1}{n}} - 1 \right] \text{ kJ/cycle}$$

$V_1 \rightarrow \text{m}^3/\text{cycle}$   
 $P_1 \rightarrow \text{kPa}$

If N is rpm

$$\text{Power} = w_{\text{cycle}} \times \frac{N}{60} \text{ (kW)}$$

Ques A single cylinder reciprocating compressor takes in air  $10 \text{ m}^3/\text{min}$  at 1 bar and  $20^\circ\text{C}$  and compresses air to a discharge pressure of 8 bar. The possible compression process are -

- polytropic compression ( $n=1.3$ )
- isentropic compression ( $n=1.4$ )
- isothermal compression ( $n=1$ )

Neglecting clearance volume for each case determine -

(a) Temp at the end of compression.

(b)  $w_s$

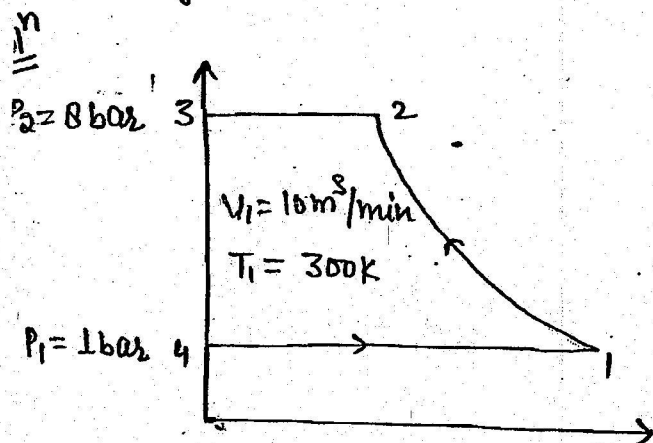
(c)  $w_c$

(d)  $w_d$

(e)  $w_{net}$

(f) Heat transfer to cylinder wall during compression.

(g) change in internal energy during compression.



1) @  $\frac{T_2}{T_1} = \left(\frac{P_2}{P_1}\right)^{\frac{\gamma-1}{\gamma}}$   $T_2 = 484.75 \text{ K}$

2)  $w_s = P_1 v_1 = 16.67 \text{ kW}$

3)  $w_c = \frac{P_2 v_2 - P_1 v_1}{\gamma - 1} = \frac{\dot{m} R (T_2 - T_1)}{\gamma - 1}$

$\dot{m} = \frac{P_1 v_1}{R T_1} = 0.1935 \text{ kg/sec}$

$w_c = 34.21 \text{ kW}$

4)  $w_d = P_2 v_2 = \dot{m} R T_2$

$w_d = 26.9 \text{ kW}$

5)  $w_{net} = w_c + w_d - w_s$   
 $= 34.21 + 26.9 - 16.67$   
 $w_{net} = 44.47 \text{ kW}$

$w_{net} = \left(\frac{\gamma}{\gamma-1}\right) P_1 v_1 \left[\left(\frac{P_2}{P_1}\right)^{\frac{\gamma-1}{\gamma}} - 1\right]$   
 $= \frac{1.3}{0.3} \times 16.67 \left[(8)^{\frac{0.3}{1.3}} - 1\right]$

$w_{net} = 44.47 \text{ kW}$

6)  $Q_{1-2} = \frac{\gamma-1}{\gamma-1} \times w_c$  Formula for closed system only  
 $= \frac{(1.4-1.3)}{1.4-1} \times (-34.21)$

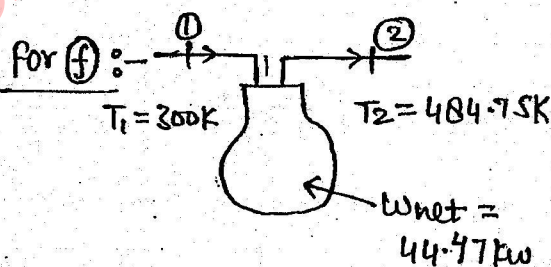
$Q_{1-2} = -8.55 \text{ kW}$

7)  $dQ = dW + dU$

$-8.55 = -34.21 + dU$

$dU = +25.6 \text{ kW}$

OR  $dU = \dot{m} c_v (T_2 - T_1)$



By SFEE

$h_1 + Q = h_2 + w_{net}$

$Q = \dot{m} c_p (T_2 - T_1) - 44.47$

$Q = -8.55 \text{ kW}$



(2) when  $n = 1.7$  :- (adiabatic)

(a)  $T_2 = 543.43 \text{ K}$

(b)  $W_s = 16.67 \text{ kW}$

(c)  $W_c = 33.79 \text{ kW}$

(d)  $W_d = 30.18 \text{ kW}$

(e)  $W_{net} = 47.30 \text{ kW}$

(f)  $Q_{1-2} = 0$

(g)  $\Delta U = -W_c = +33.79 \text{ kW}$

(3) when  $n = 1$  :- (isothermal)

(a)  $T_2 = T_1 = 300 \text{ K}$

(b)  $W_s = 16.67 \text{ kW}$

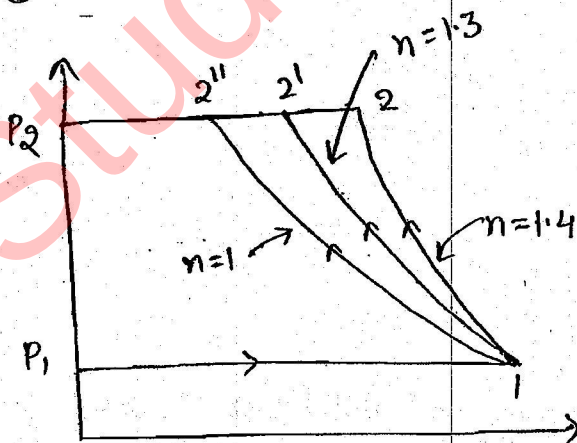
(c)  $W_c = P_1 V_1 \ln(P_2/P_1)$   
 $= 34.68 \text{ kW}$

(d)  $W_d = P_1 V_1 = P_2 V_2 = 16.67 \text{ kW}$

(e)  $W_{net} = W_c = 34.68 \text{ kW}$

(f)  $Q_{1-2} = W_c = -34.68 \text{ kW}$

(g)  $\Delta U = 0$



Practically  $n \approx 1.25$  to  $1.35$

## Isothermal efficiency

$$\eta_{iso} = \frac{\text{Isotermal work}}{\text{Actual work}} = \frac{W_{iso}}{W_{act}}$$

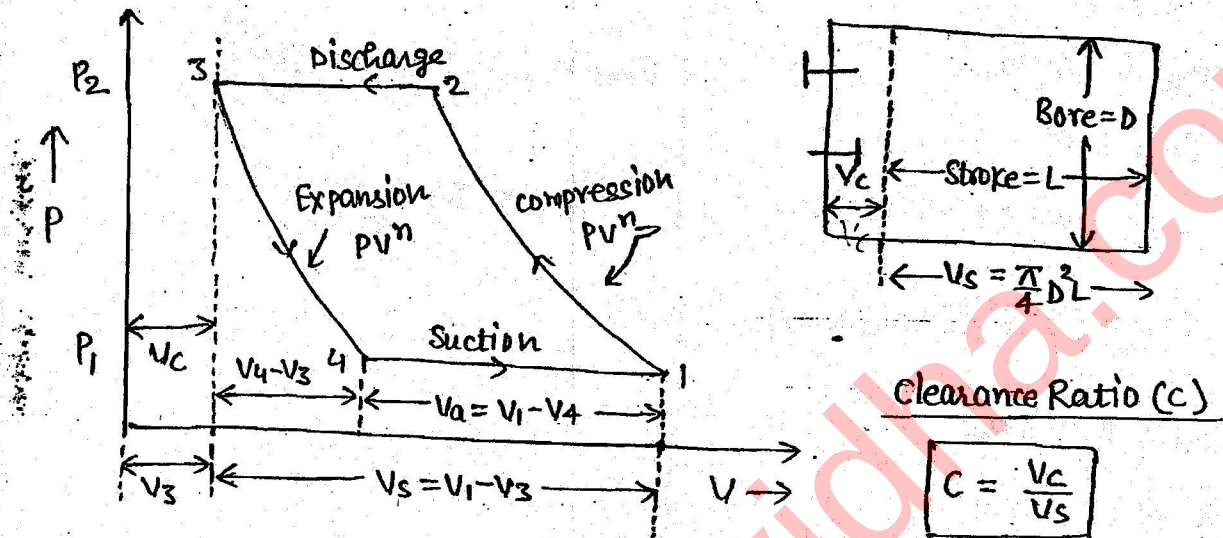
$$W_{iso} = P_1 V_1 \ln(P_2/P_1)$$

$$W_{act} = \left(\frac{n}{n-1}\right) P_1 V_1 \left[ \left(\frac{P_2}{P_1}\right)^{\frac{n-1}{n}} - 1 \right]$$

$$\eta_{iso} \approx \underline{\underline{80 \text{ to } 85\%}}$$

work input with clearance volume :-

In actual working always left a minimum volume b/w the piston and cylinder head known as clearance volume. It is provided for thermal expansion, valve tolerance and to avoid piston striking the cylinder head.



Clearance Ratio (C)

$$C = \frac{V_c}{V_s}$$

$$C \% \approx 5\%$$

workdone/cycle is given by area 1-2-3-4-1.

$$W/\text{cycle} = W_{c,1-2} - W_{c,4-3}$$

$$= \left( \frac{n}{n-1} \right) P_1 V_1 \left[ \left( \frac{P_2}{P_1} \right)^{\frac{n-1}{n}} - 1 \right] - \left( \frac{n}{n-1} \right) \left[ \left( \frac{P_3}{P_4} \right)^{\frac{n-1}{n}} - 1 \right] P_4 V_4$$

$$\text{But } P_2 = P_3 \text{ \& } P_4 = P_1$$

$$W/\text{cycle} = \left( \frac{n}{n-1} \right) P_1 V_1 \left[ \left( \frac{P_2}{P_1} \right)^{\frac{n-1}{n}} - 1 \right] - \left( \frac{n}{n-1} \right) \left[ \left( \frac{P_2}{P_1} \right)^{\frac{n-1}{n}} - 1 \right] P_1 V_4$$

$$W/\text{cycle} = \left( \frac{n}{n-1} \right) P_1 (V_1 - V_4) \left[ \left( \frac{P_2}{P_1} \right)^{\frac{n-1}{n}} - 1 \right] \text{ kJ/cycle.}$$

NOTE :- Due to clearance volume there is no change in work input required by the compressor. The only difference the actual volume of air delivered per cycle is decreased. Thus for the same volume to



be delivered no. of cycles required increases.

$$V_a \rightarrow \text{Actual Volume} = V_1 - V_4$$

$$P_1 V_a = m_a R T_1$$

$m_a = \text{actual mass.}$

Volumetric efficiency :-

It indicates the volume that is delivered during the total displacement of piston. It is ratio of actual volume of air entering the cylinder to the piston swept volume.

$$\eta_v = \frac{\text{Actual Volume}}{\text{Swept Volume}}$$

$$\eta_v = \frac{V_a}{V_s}$$

$$V_a = V_s - (V_4 - V_3)$$

$$\eta_v = 1 - \frac{V_3}{V_s} \left( \frac{V_4}{V_3} - 1 \right)$$

For expansion process 3-4

$$P_3 V_3^\gamma = P_4 V_4^\gamma$$

$$\frac{V_4}{V_3} = \left( \frac{P_3}{P_4} \right)^{\frac{1}{\gamma}} = \left( \frac{P_2}{P_1} \right)^{\frac{1}{\gamma}}$$

$$\eta_v = 1 - \frac{V_3}{V_s} \left[ \left( \frac{P_2}{P_1} \right)^{\frac{1}{\gamma}} - 1 \right]$$

as  $V_3 = V_c$  and  $\frac{V_c}{V_s} = c$

$$\eta_v = 1 - c \left[ \left( \frac{P_2}{P_1} \right)^{\frac{1}{\gamma}} - 1 \right]$$

Condition for  $\eta_v = 0\%$

$$0 = 1 - c \left[ \left( \frac{P_2}{P_1} \right)^{\frac{1}{\gamma}} - 1 \right]$$

$$\frac{P_2}{P_1} = \left[ \frac{1}{c} + 1 \right]^\gamma$$

Conclusions :-

(1) when  $P_2 = P_1$  there is no compression but  $\eta_v$  becomes 100%

(2) with increase in  $P_2$   $\eta_v$  decreases.

(3)  $\eta_v$  decreases with increase in clearance ratio.

(4)  $\eta_v$  increases with increase in expansion coefficient ( $\gamma$ ).

(5) If  $T_1 \uparrow \rightarrow \eta_v \uparrow$

$$\frac{T_2}{T_1} = \left( \frac{P_2}{P_1} \right)^{\frac{\gamma-1}{\gamma}}$$

$$\left( \frac{P_2}{P_1} \right)^{\frac{1}{\gamma}} = \left( \frac{T_2}{T_1} \right)^{\frac{1}{\gamma-1}}$$